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Oligomerization of α -olefins by the dimeric nickel bisamido complex [Ni{1-N(PMes_2)-2-N(μ -PMes_2)C₆H₄- κ^3 N,N',P,- κ^1 P'}]₂ activated by methylalumoxane (MAO)

Felicite Majoumo-Mbe^{a,c}, Peter Lönnecke^a, Victoria Volkis^b, Manab Sharma^b, Moris S. Eisen^{b,*}, Evamarie Hey-Hawkins^{a,*}

^a Institut für Anorganische Chemie der Universität, Johannisallee 29, D-04103 Leipzig, Germany ^b Shulich Faculty of Chemistry, The Institute of Catalysis Science and Technology, Haifa 32000, Israel ^c University of Buea, Faculty of Science, Department of Chemistry, Inorganic Chemistry Laboratory, P.O. Box 63, Buea, Cameroon

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ABSTRACT

The reaction of Li₂[1,2-{N(PMes₂)}₂C₆H₄], formed in situ from *n*-BuLi and the corresponding amines, with 1 equiv. of [NiBr₂(DME)] gives [Ni{1-N(PMes₂)-2-N(μ -PMes₂)C₆H₄- $\kappa^3 N$, N', P- $\kappa^1 P'$ }]₂ (1). After activation by methylalumoxane (MAO), **1** is a highly active catalyst in the oligomerization and isomerization of α -olefins such as ethene, propene, isobutene, 1-hexene and 1,5-hexadiene. For ethene oligomerization turnover frequencies (TOFs) range from 3000 to 79015 h⁻¹, depending on the reaction conditions. The TOF for propene oligomerization reaches 1190730 h⁻¹. To our knowledge, catalyst **1**, activated by MAO, is the most active catalyst for the oligomerization of propene and outperforms the best known complexes for this reaction. In the reactions with 1-hexene, 1,5-hexadiene and isobutene dimerization and isomerization products were observed.

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Catalytic polymerization and oligomerization of α -olefins, especially to give dimeric and trimeric products, are of special interest in industry [1] due to the use of olefin oligomers as building blocks and intermediates for specialty chemicals [1a,2]. In addition, olefin oligomerization is widely studied to gain better insight into the reaction mechanisms of the corresponding catalysts, because of the homogeneity of the reaction mixture and easier characterization of oligomeric products as compared to high molar mass polymers [3].

Recently, different organometallic catalysts, including homogeneous vanadium-based catalysts, zeolites, alkyl aluminum compounds, group IV and late transition metal catalysts, have been reported as good precursors for olefin oligomerization [2,4], with special focus on nickel catalysts [5].

The pronounced ability of Ni complexes for chain termination via a β -hydrogen elimination process is important for their successful application in the production of dimers and/or oligomers of ethene, propene and other olefins. Nickel catalysts have been found to be active in a wide spectrum of olefin transformations, including dimerization [6], oligomerization [7], polymerization [8], and copolymerization [9] with different comonomers. Their reduced oxophilicity and enhanced tolerance to functional groups makes them very effective in copolymerization of polar and nonpolar monomers to give new polymers with unusual microstructures [10].

Among the myriad of nickel precursors containing chelating acetylacetonate [11], 2-(diphenylamino)benzoate [12], pyrrolimine [13], salen [14], Schiff base [15], salicylideneiminato [16], and many other ligands which were found to be active for the dimerization and oligomerization of ethene and propene, the following activators are the most active: (i) catalytic systems based on a P,O chelate ligand for the production of C₄-C₂₀ oligomers from ethene, which were developed by Keim et al. and later modified in the Shell Higher Olefin Process (SHOP) for the synthesis of linear oligomers of ethene [17], (ii) P,N chelate complexes of Ni reported by Braunstein et al. [18], (iii) Grubbs' catalysts [19], and (iv) Brookhart's catalysts [20]. In addition, much attention has been focused on Ni catalysts supported on zeolites such as Y-zeolite, L-zeolite, mordenite, and mesoporous MCM-41 or on amorphous silica-alumina [21]. These systems were found to be very effective for the dimerization of ethene.

One of the industrially most important dimerization reactions is that of isobutene, as hydrogenation of the resulting dimers gives isooctane (2,2,4-trimethylpentane), which is a reference compound for the measurement of octane number that, by definition,

^{*} Corresponding authors. Tel.: +49 341 9736151; fax: +49 341 9739319 (E. Hey-Hawkins), fax: +972 4 829 5705 (M.S. Eisen).

E-mail addresses: chmoris@tx.technion.ac.il (M.S. Eisen), hey@rz.uni-leipzig.de (E. Hey-Hawkins).

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has a research octane number (RON) and motor octane number (MON) of 100. In attempts to replace the industrially used acid catalysts and ion-exchange resins for the dimerization of isobutene, some inorganic catalysts such as titanium complexes [22], organo-f-element complexes [23], and the system AlEt₃/TiCl₄ [24] were studied. However, none of them has industrial future due to the low activity compared to acidic ion-exchange resins [25].

Recently, the catalytic activity of many nickel complexes in the oligomerization of ethene was reported. For example, paramag-[NiBr₂(L)] netic complexes (L = cone-5,17-dibromo-11,23bis(diphenylphosphino)-25,26,27,28-tetrapropoxycalix-4-arene or cone-5,17-bis(diphenylphosphino)-25,26,27,28-tetrapropoxycalix-4-arene) [26] activated with methylalumoxane selectively produced 1-butene with turnover frequencies (TOFs) up to 10^6 (mol C_2H_4) (mol Ni)⁻¹ h⁻¹. Complexes with phosphinopyridine (P,N) ligands [18a] have shown TOFs for catalytic oligomerization of ethene of up to 58100 (mol C_2H_4) (mol Ni)⁻¹ h⁻¹ and 22800 (mol C_2H_4) (mol Ni)⁻¹ h⁻¹ in the presence of 6 equiv. of AlEtCl₂ and 800 equiv. of methylalumoxane (MAO), respectively. The selectivity was in the range of 70–85% for the C_4 olefins and 33–38% for 1-butene in the C₄ fraction. Nickel complexes with oxazoline- or pyridine-phosphonite ligands, as well as catalytic systems based on Ni^{II} hydrazone complexes/MAO [27] induced dimerization of ethene with good catalytic activity $(10^4 - 10^5 \text{ g mol}^{-1} \text{ h}^{-1})$ at ambient pressure. Nickel complexes with aryl-substituted α -diimine ligands activated by MAO and modified MAO (MMAO) are highly active in ethene oligomerization, with TOFs as high as 1.4×10^5 $(mol C_2H_4) (mol Ni)^{-1} h^{-1}$ [28].

Here, we report the catalytic dimerization and oligomerization of ethene, propene, isobutene, 1-hexene, and 1,5-hexadiene by the novel nickel bisamido complex [Ni{1-N(PMes_2)-2-N(μ -PMes_2)C₆H₄- κ^3 N,N',P- κ^1 P']₂ (1) activated by MAO. Complex 1 was synthesized and was characterized by various analytical techniques, including X-ray crystallography. This complex was found to be an active catalyst in the dimerization of ethene and propene, and, to the best of our knowledge, for the latter this catalyst exhibits the best activity to date. The influence of the reaction conditions on the oligomerization activity and properties of the resulting dimers and oligomers are presented.

1. Results and discussion

1.1. Synthesis and spectroscopic properties of the nickel bisamido complex $[Ni\{1-N(PMes_2)-2-N(\mu-PMes_2)C_6H_4-\kappa^3N,N',P-\kappa^1P'\}]_2$ (1)

The reaction of 1,2-{NH(PMes₂)}₂C₆H₄ [29] with 2 equiv. of *n*-BuLi in toluene at room temperature leads to the formation of the anionic ligand $[1,2-{N(PMes_2)}_{2}C_{6}H_{4}]^{2-}$, which reacts in situ with 1 equiv. of [NiBr₂(DME)] to give **1** (Scheme. 1).

In the ${}^{31}P{}^{1}H$ NMR spectrum of **1**, two doublets are observed for the two nonequivalent phosphorus atoms. The doublet at

61.8 ppm (${}^{2}J_{PP}$ = 299.4 Hz), assigned to Ni–P–N (bridging mode), is shifted to lower field in comparison to the free ligand (24.9 ppm), and the second doublet at –68.3 ppm (${}^{2}J_{PP}$ = 299.4 Hz), assigned to Ni(P–N) (chelating mode), is shifted to higher field, probably due to the effect of the small ring and the delocalization of the lone pair of electrons on nitrogen into antibonding orbitals at phosphorus, as was observed in the structures of model compounds of phosphanylamide anions [30]. A high-field shift was also observed for [TiCl₂{N(PPh₂)₂]₂] [31] (–10 ppm), a complex with P–N in a chelating mode and Ti in an octahedral configuration, whereas the chemical shift of the free ligand is 46 ppm. Details of the ¹H and ¹³C NMR spectra are given in Section 3. In the IR spectrum of **1**, the *v*(PN) band is observed at 908 cm⁻¹.

1.2. Molecular structure of 1

Violet crystals of **1** were obtained from diethyl ether/petroleum ether at 4 °C. Compound **1** crystallizes in the monoclinic space group C_2/c with four molecules of **1** and four noncoordinating diethyl ether molecules in the unit cell.

The molecular structure of **1** (Fig. 1) reveals a dimeric complex with a crystallographic C_2 axis located at the center of the hexagon formed by the two P–N bridges and the two Ni atoms. Compound **1** exhibits unusual coordination at the Ni atoms. Each Ni atom is coordinated by two nitrogen and two phosphorus atoms. The geometry around the Ni atom is highly distorted, and consists of a five-membered chelate ring via the nitrogen atoms, a three-membered chelate ring via the P–N group, and formation of a dimer in which the two rings are bridged by two phosphorus atoms. The five-membered rings have an envelope conformation in which the atoms N(1), C(19), C(24), and N(2) are coplanar, while the Ni atom lies 0.64(2) Å above this plane.

The N(1)-N(1)-N(2) bond angle of 83.6(4)° is comparable to that of 83.6(6)° observed for the chelating nitrogen donor ligands Ni-1,2-diiminophosphorane complex [NiCl₂{1,2in the $(NPPh_3)_2C_6H_4$ [32]. The sum of the bond angles [N(1)-Ni(1)-P(1) 46.0(3)°, N(1)-Ni(1)-N(2) 83.6(4)°, N(2)-Ni(1)-P(2')108.7(3)° and P(1)–Ni(1)–P(2') 123.9(1)°] of 362.3° around the Ni atom indicates a distorted planar geometry. The sum of bond angles at N(2) [C(24)–N(2)–P(2) 121.8(7)°, C(24)–N(2)–Ni 108.8(7)°, P(2)–N(2)–Ni 126.8(5)°] of 357.6° indicates trigonal-planar coordination, while at N(1) [C(19)-N(1)-P(1) 132.0(8)°, C(19)-N(1)-Ni 110.8(7)°, P(1)-N(1)-Ni 77.7(4)°] the sum of 320.7° indicates a pyramidal environment due to the chelating mode of the P-N group.

The N(1)–Ni and N(2)–Ni bond lengths of 1.872(9) and 1.965(8) Å, respectively, are shorter than those observed in other chelating N-donor Ni complexes [1.996(2)–2.017(5) Å] [32]. The shorter P(1)–N(1) bond length of 1.617(8) Å compared to the P(2)–N(2) bond length of 1.676(9) Å indicates double-bond character, as in the case of Ni complexes with iminophosphorane ligands





Fig. 1. Left: Molecular structure of **1** (H atoms omitted for clarity; thermal ellipsoids set at 50% probability); right: only the central framework is shown for clarity. Selected bond lengths (Å) and angles (°): N(1)–P(1) 1.617(8), N(1)–Ni(1)–P(1) 46.0(3), N(2)–P(2) 1.676(9), N(2)–Ni(1)–P(2') 108.7(3), N(1)–Ni(1) 1.872(9), P(1)–Ni(1)–Ni(1) 77.7(4), N(2)–Ni(1) 1.965(8), C(19)–N(1)–P(1) 132.0(8), P(1)–Ni(1) 2.197(3), C(19)–N(1)–Ni(1) 110.8(7), P(2)–Ni(1') 2.234(4), C(24)–N(2)–Ni(1) 108.8(7), P(1)–Ni(1)–P(2') 123.9(1), P(2)–Ni(1) 126.8(5), N(1)–Ni(1)–Ni(2) 83.6(4), C(24)–N(2)–P(2) 121.8(7).

[1.585(5)-1.618(2) Å] [32]. The P(1)–Ni bond of the three-membered ring is stronger than the P(2)–Ni bond of the bridging unit, as the bond length of 2.234(4) Å for the latter is larger than the 2.197(3) Å for the former. This may indicate delocalization of the nitrogen lone pair into the three-membered ring.

1.3. Oligomerization reactions promoted by complex ${\bf 1}$ activated by MAO

Complex **1** was activated by methylalumoxane prior to the oligomerization reaction. Only one broad signal at -58 ppm is observed in the ³¹P NMR spectrum for the active species.

The oligomerizations of ethene, propene, and isobutene were carried out in a high-pressure stainless steel reactor, whereas the oligomerization reactions for 1-hexene and 1,5-hexadiene were performed in Schlenk heavy duty glass vessels. For ethene, the pressure of the reactor was kept constant at 20 atm via a solenoid pressure transducer, whereas for propene and isobutene liquid monomer was used and as soon as the pressure was slightly reduced (\sim 1 atm) quenching was immediately performed. This procedure was followed to allow a constant monomer concentration in the reaction vessel and to avoid pressure-velocity polymerization side effects.

The oligomerization data for ethene, propene, and isobutene are presented in Table 2. The reactions of oligomerization/polymerization were studied as batch conditions and performing the same process at different time intervals revealed that the viscosity of the solution increases as a function of time and as the result, most of the product was formed during the first 30 min. Reactions performed for long periods of time exhibited activities much lower than the expected due to diffusivity of the monomer into the active sites with almost no change in composition of products.

It can be seen from Table 2 that the catalytic activity of complex 1 in the oligomerization of ethene increases with increasing Al:Ni ratio. In addition, the catalyst is more active in the polar solvent methylene chloride than in toluene. However, depending on the oligomerization conditions, liquid or liquid and solid products may be obtained. The formation of both oligomers and polymers with preferential selectivity for oligomers has already been reported in the literature. For example, nickel(II) complexes containing neutral N,N- and anionic N,O-bidentate ligands activated by MMAO produced a mixture of ethene trimers and polymers with moderate activity and very high selectivity towards the oligomer [33]. Tables 3 and 4 illustrate the properties of the resulting solid

Table 1	
Crystal data and stu	ucture refinement for 1

	1
Formula	$C_{84}H_{96}N_4Ni_2P_4\cdot Et_2O$
Mr	1477.07
T (K)	208 (2)
Crystal system	Monoclinic
Space group	C2/c
Ζ	4
$ ho_{\rm calc} ({ m Mg}{ m m}^{-3})$	1.271
a (Å)	16.727(4)
b (Å)	21.405(5)
c (Å)	21.843(5)
α (°)	90
β(°)	99.254(5)
γ (°)	90
$V(Å^3)$	7719(3)
Crystal size (mm)	$0.2\times0.1\times0.01$
Color, habit	Red, needle
$\mu (mm^{-1})$	0.620
F(000)	3144
Radiation	Μο Κα
$2\theta_{\min/\max}$ (°)	3.12/46.80
h,k,l ranges	$-18 \leqslant h \leqslant 14, -23 \leqslant k \leqslant 23, -21 \leqslant l \leqslant 24$
Absorption correction	SADABS
Measured reflections	16966
Independent reflections	5600
Number of parameters, restraints	445, 5
$R(F^2)$ [all data], $wR(F^2)$ [all data]	0.2569, 0.2603
$R[F^2 > 2\sigma(F^2)], wR[F^2 > 2\sigma(F^2)]$	0.1186, 0.2088
Goodness-of-fit	1.072
Extinction coefficient	0.0018(2)
$(\Delta/\rho)_{\rm max}$ (e A ⁻³)	0.484
$(\Delta/\rho)_{\rm min}$ (e A ⁻³)	-0.464

and liquid ethylene oligomerization products, respectively. The polymerization products are high density polyethylenes with similar melting points of 127.0–127.5 °C. Moreover, the higher the amount of MAO the higher the amount of the polymeric fraction obtained, but in all cases the amount of the oligomers is always much higher than that of the polymers. In the reaction with ethene, complex **1** exhibits a high activity but a low chemoselectivity as compared to previously described catalysts; it produces a mixture of dimers (where 1-butene is always the major component >77% among the dimers mixture) as well as linear (\gg 75% 1-hexene) and branched trimers (>80% 3-methyl-1-pentene) with a small preference for the linear product. The TOF exhibited for complex **1** in dichloromethane (79015 h⁻¹) is indeed higher than those

Table 2
Oligomerization/polymerization data for different olefins in the presence of complex 1 activated by MAO

Run	Substrate ^b	Ni:Al	Time (h)	Solvent	Initial temperature (°C)	Maximum temperature (°C)	Solid product ^d (g)	Liquid product (g)	Activity (g/mol cat \times h)	TOF (h ⁻¹) ^e
1	Ethene	1:100	3	Toluene	25	25	0.02	1.78	8.4×10^4	3001
2	Ethene	1:700	3	Toluene	25	25	0.11	4.61	$2.2 imes 10^5$	7868
3	Ethene	1:700	0.5	Toluene	25	25	0.06	0.86	$2.6 imes 10^5$	9202
4	Ethene	1:700	3	CH_2Cl_2	25	25	-	17.1	$8.0 imes 10^5$	28 505
5	Ethene	1:700	1	Toluene	25	25	Traces	3.53	$5.0 imes 10^5$	17653
6	Ethene	1:700	1	CH_2Cl_2	25	25	-	15.8	$2.2 imes 10^6$	79015
7	Propene	1:200	0.33	Toluene	25	50	-	25	$1.1 imes 10^7$	252580
8	Propene	1:700	0.07	Toluene	25	80	-	25	$5.0 imes 10^7$	1190734
9	Propene	1:700	0.07	CH_2Cl_2	25	80	-	25	$5.0 imes 10^7$	1190734
10	Propene	1:700	0.07	Toluene ^c	-5	0	-	25	$5.0 imes 10^7$	1190734
11	Isobutene,	1:500	3	Toluene	25	25	-	3.7	1.7×10^{5}	3084
12	Isobutene, 40 ml	1:500	3	Toluene	25	25	-	17.2	$\textbf{8.0}\times \textbf{10}^{5}$	14337

^a 10 mg of catalyst **1**.

^b Ethene 20 atm, propene 50 ml = 11 atm, 10 ml of solvent.

^c 7.6 ml of solvent.

 $^{\rm d}\,$ Clean product without catalyst or solvent.

^e mol of monomer/(mol of catalyst $\mathbf{1} \times \mathbf{h}$).

TOFs observed for the P,N chelate nickel complexes reported in the last few years [18]. However, our TOFs are somewhat lower than those obtained using Grubbs' [19] and Brookhart's [20] catalysts.

The oligomerization of propene, promoted by complex **1** and activated by MAO, was performed in liquid propene using a double jacket wall reactor with a mechanical stirrer (>100 RPM), an internal thermocouple and the reactor vessel thermostated to the requested temperature. When the oligomerization reaction was carried out at room temperature, the process was found to be extremely fast and exothermic. The pressure in the reactor dropped in a few minutes, and full conversion was reached. No solids or elastomeric materials were detected in any of the reactions with propene.

Among the many previously reported active nickel catalysts for the oligomerization of propene the following complexes are noteworthy: [Ni(COD)₂], prepared in situ and activated by MAO. polvmerizes propene with TOFs of up to 24800 h^{-1} and is regioselective towards 2,3-dimethyl-1-butene (2,3-DMB) in the C_6 fraction (>82%) [34]. [Ni(η^5 -indenyl)₂] activated by organoaluminum cocatalysts displayed an extremely high productivity (TOF up to $169000 h^{-1}$) and a moderate regioselectivity for 2,3-DMB (66.4%) [35]. Poly-salen-type Ni^{II} complexes reached TOFs of up to 221000 h^{-1} in the selective dimerization of propene [36]. An extremely high TOF of up to 268 000 h^{-1} and a rather high selectivity for dimers (95.6%) were achieved in the propene dimerization by the complex bis[N-(2,6-dimethylphenyl)-4-aminopent-3-en-2-one]nickel(II) in the presence of Et₃Al₂Cl₃ and PCy₃ [37], whereas the bis(2-hydroxy-1-naphthaldehyde)nickel system exhibited TOF of up to 262000 h⁻¹ with a moderate regioselectivity for 2,3-DMB (65.6%) [38].

As can be seen from Table 2, the nickel complex **1** is an extremely active catalyst for the oligomerization of propene. The activity increases with increasing the Al:Ni ratio. Moreover, to try to control the exothermicity of the reaction without reducing the catalytic activity we have found that when the reaction is performed at -5 °C, the temperature raised to 0 °C yielding the best turnover frequency of 1190734 h⁻¹ (run 10). Comparison of this result with the most active catalyst described in the literature allows us to conclude that for the oligomerization of propene, catalyst **1** has the highest activity to date. Under all studied conditions, complex **1** is an order of magnitude more active than the best literature catalysts [20]. Interestingly, to put the result into perspective, at room temperature and at low Al:Ni ratio, the activity of complex **1** is comparable to those catalysts reported by Wu and Lu [35–38].

Table 3 Properties of solid products of the reaction with ethene

Run	M _n	M _w	MWD ^a
1	99 000	258000	2.60
2	122000	330 000	2.70
3	1200	2400	2.20

^a MWD = molecular weight distribution = M_w/M_n .

lable 4	
Amounts of different fractions in liquid products of ethene oligomerizati	on ^a

Run	Dimer C ₄ (%)	Linear C ₆ (%)	Branched C ₆ (%)
1	82	13	5
2	87	9	4
3	85	5	10
4	49	23	28
5	77	18	5
6	54	34	12

^a GCMS and GC data.

Unexpectedly, and in contrast to the results observed for ethene, in propene the oligomerization activity is not affected by the solvent (Table 2, runs 9 and 10) presumably due to the large amount of liquid propene serving as a co-solvent. However, a very strong effect is observed for the regioselectivity of the products as presented in Table 5. For all the reactions linear and branched dimers are obtained with a slight preference for the branched compound when the reaction is performed in toluene. In all these cases where toluene was used as the solvent at both MAO/cat ratios, the product distribution is very much alike. Among the linear products 1-hexene (75%) is obtained as the major isomer along with 2-hexene (cis + trans) and 3-hexene (mostly trans), which are obtained via a simple isomerization of 1-hexene, as minor products. The amount of the isomerized dimers is an indication that the speed of formation of the dimers and trimers is by far more rapid than the isomerization process. Although lower temperatures do not lead to the formation of higher oligomers, using methylene chloride results in the partial formation of C_9-C_{12} oligomers without changing the activity (Table 2, runs 8 and 9). Interestingly, the distribution of the products for the dimers remains almost unchanged but for the branched trimer 2,3-DMB is the major isomer (>82%). For the higher oligomers a myriad of isomers were obtained.

Table 5Fractions in the liquid products of propene oligomerization

Run	Linear C ₆ (%)	Branched C ₆ (%)	Higher oligomers
7	46	54	-
8	41	59	-
9	59	12	C ₉ -C ₁₂ (29%)
10	47	53	-

 Table 6
 Oligomerization^a data for 1-hexene and 1,5-hexadiene with the complex 1

Run	Substrate ^b	Ni:Al	Solvent	Time (h)	Product (g)	Activity (g/ mol cat \times h)	TOF (h ⁻¹) ^c
1	1-Hexene	1:500	Toluene	4	2.4	$\textbf{8.4}\times10^4$	1000
2	1-Hexene	1:500	CH_2Cl_2	4	3.1	$1.1 imes 10^5$	1292
3	1,5- Hexadiene	1:500	Toluene	4	1.2	$\textbf{4.2}\times 10^4$	512
4	1,5- Hexadiene	1:500	CH ₂ Cl ₂	4	4.8 (wax) Dimers (60%) trimers (40%)	1.7 × 10 ⁵	2050

^a 10 mg of catalyst 1, RT.

^b 5 g of substrate.

^c mol of monomer/(mol of Catalyst $\mathbf{1} \times \mathbf{h}$).

The reaction of **1**/MAO with isobutene was also studied in a high-pressure reactor at room temperature. Although the TOFs were not very high for these reactions as compared to propene, but the selectivity was remarkable, only one dimeric product (2,5-dimethyl-3-hexene) was produced (Table 2).

Complex 1 was also found to be active in the oligomerization of 1-hexene and 1,5-hexadiene (Table 6). For these olefins, the reaction in toluene was again slower than for ethene and propene and as compared in dichloromethane a similar behavior is obtained inducing slightly to better activities in the more polar solvent. In toluene the selectivity was exclusively for dimers for both substrates whereas for dichloromethane trimers were obtained for 1.5-hexadiene. For 1-hexene in both solvents, the linear 1-dodecene was the major product (>75%) but isomerization of the double bond to different diastereomers is observed producing a myriad of products as a function of time which were difficult to separate or compare. For 1,5-hexadiene, the dimer 5-methyleneundeca-1,10diene is obtained as the major isomeric product (>50%) but a number of compounds are also observed. In dichloromethane, a mixture of dimers and trimers was obtained as a low melting wax. Important to note that for 1,5-hexadiene in both solvents, no cyclic oligomers were obtained.

2. Conclusions

The anionic ligand $[1,2-{N(PMes_2)}_2C_6H_4]^{2-}$ was produced by the reaction of 1,2-{NH(PMes_2)}_2C_6H_4 with 2 equiv. of *n*-BuLi in toluene at room temperature. Treating the latter *in situ* with 1 equiv. of [NiBr₂(DME)] resulted in the formation of precatalyst **1**, which was characterized by NMR spectroscopy and X-ray diffraction.

The activation of complex **1** in toluene or dichloromethane by an excess of MAO results in the formation of species which are extremely active in the oligomerization of ethene and propene. For ethene oligomerization high TOF numbers were obtained and for propene TOFs of up to 1.2×10^6 h⁻¹ was obtained. To the best of our knowledge, catalyst **1** activated by MAO exhibits the largest activity to propene oligomerization to date. In addition, the activated complex **1** was also found to be highly effective in the dimerization reactions of 1-hexene, 1,5-hexadiene, and isobutene.

3. Experimental

All reactions were carried out in an atmosphere of dry nitrogen using standard Schlenk or vacuum line techniques. The solvents were purified (diethyl ether, THF, toluene: reflux over Na/benzophenone; petroleum ether: reflux over LiAlH₄) and distilled under nitrogen. The infrared spectrum was recorded on a Perkin-Elmer System 2000 FT-IR spectrometer scanning between 400 and 4000 cm⁻¹ using KBr disks. The chemical shifts for the ¹H and ¹³C NMR spectra are reported in parts per million (ppm) at 400.13 and 100.63 MHz, respectively, with tetramethylsilane as external standard. The chemical shifts for the ³¹P NMR spectrum are reported in ppm at 161.97 MHz, with 85% H₃PO₄ external standard. The FAB mass spectrum was recorded on a ZAB-HSQ-VG with 3-nitrobenzyl alcohol as matrix. The elemental analyses were recorded on a VARIO EL (Heraeus). The melting point was determined in a sealed capillary and was not corrected. The 2.50 M solution of *n*-BuLi in *n*-hexane (Aldrich) was used as purchased. [NiBr₂(DME)] was prepared according to the literature [39].

Crystallographic data of **1** are listed in Table 1. The data were collected with a Siemens CCD ($_{SMART}$) diffractometer using ω -scan rotation. Data reduction was performed with $_{SAINT}$ including the program $_{SADABS}$ for empirical absorption correction [40]. The structure was solved by heavy-atom methods and the refinement of all non-hydrogen atoms was performed with $_{SHELX97}$ [40]. Due to the weakly diffracting, small crystal, the quality of our experimental results are relatively poor, although they are good enough for a structural confirmation of **1**. The presentation of the molecular structure in this paper was generated with ORTEP [40].

3.1. $[Ni\{1-N(PMes_2)-2-N(\mu-PMes_2)C_6H_4-\kappa^3N,N',P,-\kappa^1P'\}]_2$ (1)

n-BuLi (1.1 ml, 2.23 M in *n*-hexane) was added dropwise to a solution of 1,2-{NH(PMes₂)}₂C₆H₄ (0.8 g, 1.24 mmol) in toluene (25 ml). The mixture was stirred for 3 h, and then added dropwise to a solution of [NiBr₂(DME)] (0.38 g, 1.23 mmol) in toluene. The reaction mixture was stirred overnight, and then filtered. The solvent was removed, and the residue was dissolved in diethyl ether. The solution was concentrated and layered with petroleum ether. The product was obtained as violet crystals at 4 °C. Yield: 0.58 g (68%), M.p.: 255–257 °C. ¹H NMR (C₆D₆, ppm): 7.39 (br, s, 2H in C₆H₄), 7.04 (br, s, 2H in C₆H₄), 6.90 (br, s, 2H, C₆H₄), 6.63 (s, 8H, *m*-H in Mes), 6.53 (s, 8H, *m*-H in Mes), 6.10 (br, s, 2H in C₆H₄), 3.57 (s, Et₂O), 2.73 (s, 24H, o-CH₃ in Mes), 2.74 (s, 24H, o-CH₃ in Mes), 2.00 (s, 12H, p-CH₃ in Mes), 1.92 (s, 12H, p-CH₃ in Mes), 1.42 (s, Et₂O). ³¹P NMR (C₆D₆, ppm): 61.8 (d, ² J_{PP} = 299.4 Hz), -68.3 (d, ${}^{2}J_{PP}$ = 299.4 Hz). ${}^{13}C{}^{1}H$ NMR (CD₂Cl₂, ppm): 142.3 (d, ${}^{2}J_{PC}$ = 11.2 Hz, o-C in Mes), 141.4 (s, p-C in Mes), 140.2 (d, ${}^{2}J_{PC}$ = 11 Hz, o-C in Mes), 140.02 (s, p-C in Mes), 134.3 (d, ${}^{2}J_{PC}$ = 11.2 Hz, C₆H₄), 133.6 (d, ${}^{2}J_{PC}$ = 19.4 Hz, C₆H₄), 131.6 (d, ${}^{1}J_{PC}$ = 38.2 Hz, *ipso-C* in Mes), 131.7 (d, ${}^{1}J_{PC}$ = 38.0 Hz, *ipso-C* in Mes), 130.7 (d, ${}^{3}J_{PC}$ = 7.6 Hz, *m*-C in Mes), 130.2 (d, ${}^{3}J_{PC}$ = 9.7 Hz, m-C in Mes), 122.2 (br, s, C₆H₄), 121.8 (br, s, C₆H₄), 120.4 (s, C_6H_4), 120.2 (d, ${}^{3}J_{PC} = 3.3$ Hz, C_6H_4), 120 (s, C_6H_4), 119.1 (d, ${}^{3}J_{PC} = 4.9$ Hz, C_6H_4), 67.7 (s, Et₂O), 25.5 (s, Et₂O), 24.2 (d, ${}^{3}J_{PC} = 7.8$ Hz, o-CH₃, in Mes), 22.6 (d, ${}^{3}J_{PC} = 9.9$ Hz, o-CH₃ in Mes), 20.9 (s, *p*-CH₃ in Mes), 20.6 (s, *p*-CH₃ in Mes). IR (KBr, cm⁻¹): 3022w, 2923vs, 2923vs, 1602vs, 1554m, 1493vs, 1456vs, 1401vs, 1304vs, 1261m, 1031vs, 908m, 850s, 803s, 739s, 638m, 553m, 441s. MS (FAB) [m/z, %]: 701.4 [M⁺/2, 77], 643.4 [M⁺/2-Ni, 10], 373.2 [M⁺/2-NiPMes₂, 38], 269 [(Mes₂P)⁺, 52], calc. for

 $C_{84}H_{96}N_4Ni_2P_4$: *M* = 1403.00. Anal. Calc. for $C_{84}H_{96}N_4Ni_2P_4 \cdot 40Et_2$ (1699.49): C, 70.7; H, 8.0; N, 3.3. Found: C, 70.0; H, 9.4; N, 3.2%.

3.2. Reaction of complex **1** with ethene

In a glove box a high-pressure reactor (100 ml) was charged with complex **1** (10 mg, 7.13×10^{-3} mmol), the desired amount of MAO according to the Ni:Al ratio, and 10 ml of solvent. Then the reactor was connected to a high-pressure line and filled with ethene (99.999%) at 20 atm. To maintain a constant pressure of 20 atm a solenoid valve was used. Hence, when the pressure in the reactor was reduced it was refilled constantly. After a specific amount of time, the reactor (kept at $-30 \circ C$) was opened in a well-ventilated hood, the raw content was weighed, and the amount of products was calculated as the difference between the mass of raw content and the sum of the masses of the catalyst. MAO, and the solvent. The raw product was maintained at -30 °C to keep the C₄ fraction liquid and filtered. From the resulting liquid samples for NMR and GCMS were taken. The solid material obtained at room temperature was washed with a 1:1 mixture of methanol and HCl (10 wt% solution), filtered again, washed with acetone, and dried under vacuum.

3.3. Reaction of complex **1** with propene

In a glove box, a high-pressure stainless steel reactor (100 ml) was charged with complex **1** (10 mg, 7.13×10^{-3} mmol), the desired amount of MAO according to the Ni:Al ratio, and 10 ml of solvent. The reactor was connected to a high-vacuum line, and propene (50 ml, 25 g) was transferred to the reactor (propene was frozen with liquid nitrogen, and the volume measured in a heavy-duty, calibrated glass vessel). The reactor was brought to room temperature and the mixture was stirred during the reaction time. At the beginning of the reaction the pressure of propene was 10–11 atm. A quick and exothermic reaction occurred, the pressure dropped to zero, and the reactor was opened. Immediately after opening the reactor the raw content was weighed and the amount of products was calculated as the difference between the mass of the raw contents and the sum of the masses of the catalyst, MAO, and the solvent. The raw product was filtered off. From the resulting liquid, samples were taken for NMR and GCMS.

3.4. Reaction of complex **1** with 1-hexene and 1,5-hexadiene

These reactions were carried out in a Schlenk tube, charged in a glove box with catalyst **1** (10 mg, 7.13×10^{-3} mmol), the desired amount of MAO according to the Ni:Al ratio, and 10 ml of solvent. Then the Schlenk tube was connected to a vacuum line, and a measured amount of the substrate was injected into the vessel via a gas-tight syringe. After the reaction mixture was stirred for an adequate amount of time, the products were separated as follows: a 1:1 mixture of methylene chloride and HCl (10 wt% in water) was added to the Schlenk tube. After neutralization of the catalytic mixture with solid NaHCO₃, the content of the Schlenk tube was transferred to a separating funnel. The organic fraction was separated and dried with MgSO₄. After filtration the vessel was connected to a flash evaporator, and methylene chloride was removed by vacuum. The resulting residue was analyzed by NMR and GCMS.

3.5. Reaction of complex 1 with isobutene

The reactions were carried out in a high-pressure stainless steel reactor (100 ml) charged in a glove box with complex 1 (10 mg, 7.13×10^{-3} mmol), the desired amount of MAO according to the Ni:Al ratio, and 10 ml of solvent. Then, the reactor was connected

to a vacuum line, and a measured amount (10 ml or 40 ml) of isobutene was transferred under vacuum to the reactor (by a similar procedure as for propene but at -30 °C). After the reaction was finished the excess of isobutene was released in a well-ventilated hood. The products were separated similar to the procedure described for 1-hexene: a 1:1 mixture of methylene chloride and HCl (10 wt% in water) was added to the Schlenk tube. After neutralization of the catalytic mixture, the contents of the Schlenk tube were transferred to a separating funnel. The organic fraction was separated and dried with MgSO₄. After filtration the mixture was analyzed by NMR and GCMS.

4. Supplementary material

CCDC 652339 contains the supplementary crystallographic data for this paper. These data can be obtained free of charge from The Cambridge Crystallographic Data Centre via www.ccdc.cam.ac.uk/ data_request/cif.

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